

REMARKS

Claims 1-4, 6-7, and 9-17 are pending in the application. Claims 1-4 and 6-7 have been amended. Claims 5 and 8 have been cancelled and new claims 9-17 have been added.

The specification has been amended to more clearly describe the zones shown in the drawings. See, e.g. Figures 1 and 2. No new matter has been added.

Proposed drawing corrections to Figures 1-3 are shown in red. Specifically, reference number 14 identifying the intermediate zone and reference number 12 identifying the hot zone have been added. No new matter has been added.

Claims 1, 2 and 6 were objected to because of informalities. The informalities identified by the Examiner have been corrected.

Claims 1 – 8 were rejected under 35 USC §112, second paragraph as being indefinite. Independent claims 1 and 2 have been amended to more clearly define the zones. Support for these amendments can be found in the Specification as filed at pages 3-4 and Figures 1 – 3.

Claim 3 has been amended to recite a “duct” rather than a means for supply. Support for this amendment can be found at the Specification as filed at p. 3.

Claims 4 and 7 have been amended to define structural limitations. Accordingly these claims are no longer indefinite.

Claims 1, 3 – 5 were rejected under 35 USC § 102(b) as being anticipated by US Patent No. 5589142 (*Gribbon*), claim 1 recites

Equipment for the purification of gases comprising at least one heat exchanging matrix, said matrix adapted to heat the gas in a regenerative process to oxidation or decomposition temperature, the at least one heat exchanging matrix comprising three zones, one zone is a catalytic zone having a temperature below the oxidation or decomposition temperature that is catalytically active in promoting reduction of nitrogen, one zone is a combustion zone having a temperature of at least the oxidation or decomposition temperature, and one zone is an intermediate zone, said catalytic zone is separated from said combustion zone by said intermediate.

Gribbon does not teach or suggest equipment with all the limitations of claim 1. In *Gribbon*, the catalytic beds 22, 24 are located next to the heating zone. See, e.g. Fig. 1 Col. 2 lines 25-30 and Col. 2, line 1- Col. 4, line 30. There is no teaching or suggestion on an intermediate zone between the hot zone and the catalytic zone. The regenerator beds 14, 16 are not catalytic zones. See, e.g. Col. 2 lines 60-62. In the intermediate bed zone the temperature can rise to an oxidation and decomposition temperature which is much higher than the catalyst could withstand and after the hot zone (counted in the stream direction) there is a second bed zone in which the temperature is allowed to fall again to a temperature which will not destroy the catalyst. Thus, *Gribbon* does not teach

or suggest locating the catalytic zone away from the hot zone. It teaches locating the catalytic zone close to the hot zone.

Further, the self-combustion of the present invention occurs at very high temperatures close to the hot zone. The catalytic zone(s) are arranged a distance from the hot zone where the temperature has fallen below a point where the catalytic material will not be damaged. The reverse situation exists in *Gribbon*, the *Gribbon* device locates the catalytic beds close to the heater. *Gribbon* does not teach or suggest a device with all the limitations of Claim 1. Thus, independent claim 1 and claims 3-4 are patentable.

Claims 1 and 2 were rejected under 35 USC § 102(b) as being anticipated by US US Patent No. 5262131 (*Bayer*), claim 1 recites:

Equipment for the purification of gases comprising at least one heat exchanging matrix, said matrix adapted to heat the gas in a regenerative process to oxidation or decomposition temperature, the at least one heat exchanging matrix comprising three zones, one zone is a catalytic zone having a temperature below the oxidation or decomposition temperature that is catalytically active in promoting reduction of nitrogen, one zone is a combustion zone having a temperature of at least the oxidation or decomposition temperature, and one zone is an intermediate zone, said catalytic zone is separated from said combustion zone by said intermediate.

and claim 2 recites:

Equipment for the purification of gases comprising a single heat exchanging matrix said matrix adapted to heat the gas in a regenerative process to oxidation or decomposition temperature, the heat exchanging matrix comprising two catalytic zones that are catalytically active and situated on each side of a center combustion zone of the matrix and two intermediate zones, each catalytic zone is separated from the center combustion zone by one of the intermediate zones and each catalytic zone has a temperature below the oxidation or decomposition temperature.

In *Bayer* "The air passing through the central gravel region 40 continues to be heated, however, by the coil 42 and thereby reaches the maximum temperature substantially as it enters the upper catalyst layer 38, where the most of the oxidation occurs" (column 4 lines 3-7). Consequently the streaming medium has its highest temperature when it reaches the catalyst (see also column 4 lines 43-44). Thus, *Bayer* does not teach or suggest equipment for the purification of gases with all the limitations of Claim 1 or 2 including a catalytic zone with temperatures below the oxidation temperature.

Claims 1 - 8 were rejected under 35 USC §103(a) as being obvious over *Gribbon* in view *Bayer*. *Gribbon* does not teach or suggest equipment with all the limitations of claim 2. In *Gribbon* the catalytic beds 22, 24 are located next to the heating zone. See, e.g. Fig. 1 Col. 2 lines 25-30 and Col. 2, line 1- Col. 4, line 30. The regenerator beds 14, 16 are not catalytic zones. See, e.g. Col. 2 lines 60-62. Thus, *Gribbon* does not teach or suggest locating the catalytic zone away from the hot zone. It teaches locating the hot

catalytic zone close to the zone. *Gribbon* does not teach or suggest separating the catalytic zone from the hot zone. The self-combustion of the present invention occurs at very high temperatures. The high temperatures exist in the hot zone and may also exist in the intermediate zone. The catalytic zone(s) are arranged a distance from the hot zone where the temperature has fallen below a point where the catalytic material will not be damaged. The reverse situation exists in *Gribbon*, the *Gribbon* device locates the catalytic beds close to the heater. Because the catalytic zones are next to the hot zone, the temperature in the catalytic zone can be above the oxidization temperature.

Bayer does not make up the deficiencies in *Gribbon*. The hottest temperature is in the catalytic zone. Thus, independent claims 1 and 2 and claims 3-4 and 6-7 are patentable.

CONCLUSION

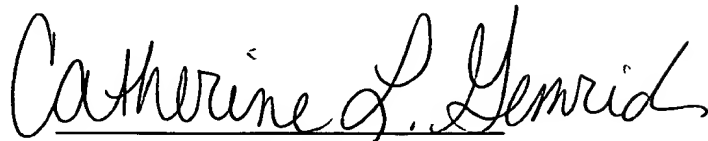
Applicant asserts that all of the objections have been obviated and, therefore now respectfully requests withdrawal of the objections, and allowance of the application.

REQUEST FOR EXTENSION OF THE TERM

Applicant respectfully requests an extension of the normal term that expired on 14 January 2005, for two months, to 14 March 2005.

The Commissioner is hereby authorized to charge Deposit Account Number 04-2219 \$450 to cover the cost of the extension. Any deficiency or overpayment should be charged or credited to Deposit Account Number 04-2219, referencing our Docket Number 11761.

Respectfully submitted,




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CERTIFICATE OF MAILING

I hereby certify that this correspondence is being deposited with the United States Postal Service as first class mail in an envelope addressed to: Commissioner of Patents and Trademarks, Alexandria, VA 22313-1450, on March 14, 2005.


Katherine Bruce

SPECIFICATION AMENDMENTS

SPECIFICATION WITH MARKINGS TO SHOW CHANGES MADE

Background of the Invention

Field of the Invention

The present invention relates to a device for pollution control. More specifically, the present invention relates to device for pollution control where a polluted stream of air or gas is purified from both oxidisable material and nitrogen oxides simultaneously by a combination of regenerative high temperature treatment and catalytic treatment.

Description of Related Art

Polluted air and other gases can be purified by heat treatment to such temperatures that the pollutants are oxidised or decomposed. US patent 4 267 152 and US patent 4 741 690 describes such processes where the polluted gases are fed through regenerative devices where the heating of a gas is immediately followed by cooling and recovery of the heat content of the gas. In this way heat treatment of the gas to a high temperature can be made in an economical way without a high expenditure of energy.

The incoming raw gas is in these processes successively heated to the high temperature by means of contact with a matrix of solid material capable of heat transfer to the gas. In the solid matrix there is a temperature gradient so that the gas is first successively heated to a maximum temperature. After attaining its maximum temperature the gas is then cooled in an analogous manner by means of contact with a solid matrix of successively lower temperature. In US patent 4 287 152 the heating and the cooling matrices are separated from each other but used alternatively for heating and cooling purposes according to an alternating direction of gas flow through the matrices. The different matrices are alternatively used for heating and cooling of the gas. In US patent 4 741 690 there is only one continuous matrix through which the gas flow is being fed. The temperature profile in this matrix is such however that when the gas passes through it is first successively heated to a maximum temperature and then successively cooled.

In both cases the operation is regenerative and the gas is fed in alternating directions through the equipment and is successively first heated to a maximum temperature and then cooled. The maximum temperature employed is such that it is at or above the temperature that is necessary for the intended oxidation or decomposition reaction to take place.

Processes and equipment like these are extensively used for the purification of ventilation air from painting and printing processes. It can also be used for the purification of exhaust gases from internal combustion engines. In this and other cases

nitrogen oxides are a part of the pollution problem.

For diesel engines the concentration of nitrogen oxides in the exhaust can reach several thousands of ppm. Good reduction of these nitrogen oxides can be accomplished if the exhaust is first mixed with a corresponding amount of ammonia, urea or other amine compound before it is heat treated in the above described manner. During the heating the mixture will pass through the relevant temperature window for a selective non catalytic reduction (SNCR) reaction where the nitrogen oxides and the amines are transformed to elemental and harmless nitrogen.

Diesel engine exhaust for example can thus be purified in the above described process first during the heating phase when nitrogen oxides are removed and then at the high temperature when soot, aldehydes and other organic matter is oxidised. This way of operation of the equipment is described in European patent number EPC 609 288.

Experience has shown that when the original concentration of nitrogen oxides is more than 1000 ppm a good reduction can be achieved and the concentration nitrogen oxides brought down to a couple of hundred ppm. However when the original concentration already is in this low region as for example in the exhaust from lean burn natural gas engines reduction is very poor.

Summary of the Invention

The present invention constitutes a way of improving this situation so that the concentration of nitrogen oxides in the outgoing treated gas can be brought down significantly below 50 ppm. The improvement is accomplished by the incorporation of catalytically active zones into the heat transfer matrices of earlier designs.

Device for pollution control where a polluted stream of air or gas is purified from both oxidisable material and nitrogen oxides simultaneously by a combination of regenerative high temperature treatment and catalytic treatment.

Brief Description of the Drawings

Figure 1 is a cross section of a pollution control device.

Figure 2 is a cross section of an alternative pollution control device.

Figure 3 is a cross section of an alternative pollution control device.

Detailed Description of the Invention

An embodiment of the invention is described in figure 1 and another embodiment of the invention is described in figure 2. In both figures, 1 is a valve mechanism for the direction of air (gas) in alternating directions through the equipment. 2 and 3 are connecting ducts for incoming raw and outgoing cleaned gas respectively. 4 and 5 are wind boxes for distribution and collection of air (gas) that goes through the heat transfer matrix 6. In the design shown in figure 2—1 this matrix is

divided into two parts 6 and 6' surrounding a combustion chamber 7 which is absent in the design shown in figure 2 where the heat exchanging matrix stretches all the way between the two wind boxes 4 and 5. Both designs comprises means for heating in a hot zone 12: in figure 1 in the form of electric heaters 8 and in figure 2 in the form of a burner 9. Both designs also incorporate catalytically active zones 10 and 11 within the heat exchanging matrices. The catalytically active zones are sperated from the hot zone 12 by at least one intermediate zone 14. In the design of figure 1, the temperature is high in the centrecenter, or not zone 12, of the heat exchanging matrix 6 and gradually decreases towards top and bottom. In the design in figure 2 the temperature is high in the hotzone/ or in the combustion chamber 7, 12 and the upper parts of the intermediate zones 14 of heat exchanging matrixes 6 and 6'. The and the temperature gradually decreases towards the bottom of the heat exchanging matrices. By regenerative heat exchange and regular switching of the direction of flow through the equipment these temperature patterns can be generally maintained without excessive heat demands being put on the heating means 8 (figure 1) and 9 (figure 2). When the oxidation of pollutants in the gas stream produces enough energy they can be switched off altogether.

In operation raw polluted gas is first mixed with ammonia, urea, or other compound able to act as a selective nitrogen oxides reducing agent. The mixture is then introduced into a cold end of a heat exchanger matrix and by passing through it is successively heated to oxidation or decomposition temperature which is attained in the inner part of the equipment i.e. the hot centre-center of the matrix in fig 1 including the hot zone 12 and at least a protion of the intermediate zone 14 or the intermediuate zone 12 at the uppermost parts of the matrices 6 and 6' and the combustion chamber hot zone 7, 12 in fig 2. Before reaching this high temperature however the mixture is passed through the catalytically active zone 10, 11 of the heat exchanger matrix 6 or 6'. Here nitrogen oxides react with the mixed in reducing agent and are thus removed. The catalytic zone 10, 11 is placed in the heat exchanging matrix in such a way that the temperature conditions there are favourable for this reduction and a selective catalytic reaction (SCR) takes place. The reaction takes place at a substantially lower temperature than an SNCR reaction and this together with the use of catalyst makes a more thorough reduction possible as compared with an operation according to European patent EPC 609 288 and lower levels of concentration of nitrogen oxides are obtainable. When the inlet concentration of nitrogen oxides is low the difference becomes significant.

After the SCR reaction the gas mixture is further heated and as in European patent EPC 609 288 other pollutants as well as any remaining surplus of reduction

agents are destroyed in the hot inner part.

In operation of regenerative equipment like this the direction of gas through the equipment is reversed at regular intervals. Unless special precautions are taken, at every change in flow direction some untreated gas mixture is being "short circuited" or carried over to the outlet. It is then advantageous to interrupt the supply of reducing agent for a short period before such changes in flow direction. Unnecessary emissions of reducing agent is then avoided.

An important aspect of the invention is that catalyst can be applied in such a way that the reducing activity of the catalyst is retained for a considerable time after the supply of reducing agent has been interrupted. The overall reduction efficiency of the equipment thus is not disadvantageously affected by such interruptions in the supply of reducing agent. This effect can be so pronounced that the equipment can be modified to comprise only one zone of catalytically active material. This zone is then activated by the supply of reducing agent when this part of the equipment is used as inlet end for the gas stream. When the gas stream is reversed and the active zone is at the outlet end of the equipment the supply of reducing agent is cut off and the reduction of nitrogen oxides takes place in this zone after the high temperature treatment. Figure 3 shows such a design with only one catalytically active zone 10.

The invention has been described above in the conjunction with regenerative equipment using either one heat exchanging matrix or two different matrices surrounding a combustion chamber. There also are designs using three or more heat exchanging matrices surrounding a common combustion chamber. In some designs the direction of flow through the heat exchanging matrix is changed only gradually in the heat exchanging matrix so that different parts of the same matrix have flow in different directions. This is obtained for instance by rotation of a matrix versus fixed inlet and outlet ports or by the use of a rotating valve system working together with a fixed matrix. Together all these different designs are often called regenerative thermal oxidisers (RTOs). In all the different designs the heat exchanging matrix material is subject to a gas flow that is reversed at regular intervals and the incoming gas is successively heated to a high temperature where oxidation and decomposition takes place. The invention is applicable in all these cases. The design shown in figures 1 and 3 have the advantage that the equipment is compact and can be made comparatively small which very often is an important aspect when used in various conjunctions together with internal combustion engines.

Catalytically active zones can be incorporated in at least one of the matrices and be activated by regular supply of reducing agent. As described above this supply does not have to be continuous. In some cases the raw gas may already contain such

reducing agents or the catalyst or combination of catalyst and raw gas be such that no such supply is necessary.